

Ozone decomposition on Saharan dust: an experimental investigation

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Abstract. The heterogeneous reaction between O₃ and authentic Saharan dust surfaces was investigated in a Knudsen reactor at ≈ 296 K. O₃ was destroyed on the dust surface and O₂ was formed with conversion efficiencies of 1.0 and 1.3 molecules O₂ per O₃ molecule destroyed for unheated and heated samples, respectively. No O₃ desorbed from exposed dust samples, showing that the uptake was irreversible. The uptake coefficients for the irreversible destruction of O₃ on (unheated) Saharan dust surfaces depended on the O₃ concentration and varied between 3.5×10^{-4} and 5.5×10^{-6} for the initial uptake coefficient ($\gamma_0 \approx 3 \times 10^{-5}$ at 30 ppbv O₃ STP) and between 4.8×10^{-5} and 2.2×10^{-6} for the steady-state uptake coefficient ($\gamma_{ss} \approx 7 \times 10^{-6}$ at 30 ppbv O₃ STP). At very high O₃ concentrations the surface was deactivated, and O₃ uptake ceased after a certain exposure period. Sample re-activation (i.e. de-passivation) was found to occur over periods of hours, after exposure to O₃ had ceased, suggesting that re-activation processes play a role both in the laboratory and in the atmosphere.

1 Introduction

Between 1600 and 2000 Tg of mineral aerosol are predicted to be uplifted annually into the atmosphere (Ginoux et al., 2001). The major source areas of the world are situated in a broad band that extends from the west coast of North Africa, across the Arabian Peninsula to central Asia, approximately in the 10° N–28° N latitude band (e.g. Prospero, 1999). Mineral aerosol is uplifted from so-called “hot spots” (Gillette, 1999) into the atmosphere by strong surface winds that travel behind cold frontal systems (Carmichael et al., 1996). Particles smaller than 10 μ m have atmospheric lifetimes of several days (Prospero, 1999) and can be transported over thou-

sands of kilometres across the N. Atlantic and the N. Pacific (Duce et al., 1980; Savoie and Prospero, 1982), travelling mainly at heights between 3 and 7 km (Prospero et al., 1981; Husar et al., 1997).

Mineral dust is frequently associated with nitrate and sulphate, the concentrations of which can increase with transport time (e.g. Savoie and Prospero, 1982; Savoie et al., 1987; Prospero and Savoie, 1989; Okada et al., 1990), implying that mineral aerosol may provide a reactive surface able to support heterogeneous processing of trace gases. Early modelling studies (Zhang et al., 1994; Dentener et al., 1996) have considered the possibility that mineral aerosol can influence the tropospheric budgets of important trace gases (O₃, NO_y, HO_y), and identified the potential role of mineral dust in modifying photochemical cycles on a global scale. Recently, field observations of reduced O₃ concentrations in a mineral aerosol plume were interpreted as resulting from direct uptake of O₃ on the dust particle surface (50%) with the rest resulting from changes in NO_y (de Reus et al., 2000).

The catalytic destruction of O₃ has been subject of scientific interest for more than 40 years because of its toxicity (Ouederni et al., 1996; Dhandapani and Oyama, 1997). A number of studies have been performed on the adsorption of O₃ onto various mineral oxides, using electron paramagnetic resonance, infrared spectroscopy and kinetic measurement techniques (Dhandapani and Oyama, 1997). The surfaces examined were among others: γ -Al₂O₃ (Klimovskii et al., 1983; Bulanin et al., 1995a; Thomas et al., 1997), SiO₂ (Bulanin et al., 1994), TiO₂ (Bulanin et al., 1995a, 1995b), CaO (Bulanin et al., 1997) and MgO (Bulanin et al., 1995a; Berlier et al., 2002). A few semi-quantitative studies on the interaction between ozone and authentic mineral dust have been published (Suzuki et al., 1979; Alebic-Juretic et al., 1992; Alebic-Juretic et al., 2000), and initial uptake coefficients for O₃ uptake onto synthetic and authentic minerals have been measured (Michel et al., 2002).

The interaction of ozone with mineral dust is also impor-

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Table 1. Knudsen reactor parameters

Knudsen reactor parameter	Value	
volume	V	120 cm^3
temperature	T	296 K
total pressure	p	$< 1 \text{ mTorr}$
O_3 number density		$3.1 \times 10^{10} \text{ to } 1.7 \times 10^{13} \text{ cm}^{-3}$
O_3 flow		$3.0 \times 10^{12} \text{ to } 1.7 \times 10^{15} \text{ s}^{-1}$
escape orifice diameter	d	3.5 mm
escape orifice escape rate	k_{esc}	$0.3257 (T/M)^{1/2} \text{ s}^{-1} *$
surface area of sample support	A_s	$1.0 \text{ and } 2.25 \text{ cm}^2$
O_3 sample collision frequency	ω	$75.5 \text{ and } 170.0 \text{ s}^{-1}$

* T in K, M in atomic mass units

tant in the context of chemical ageing or activation of the surface which could modify the heterogeneous behaviour of other trace gases. In the present study we examine experimentally a number of aspects of the interaction of O_3 with Saharan dust surfaces.

2 Experimental section

The experimental set-up has been described in detail before (Hanisch and Crowley, 2001), and only salient features and modifications are reproduced here. The gas-mixing facility, Knudsen reactor and mass spectrometer are shown schematically in Fig. 1.

2.1 Knudsen reactor / mass spectrometer

The stainless steel Knudsen reactor consists of a main compartment and a sample compartment ($296 < T / \text{K} < 450$) which can be separated by an isolation plate. All interior parts and walls of the Knudsen reactor are coated with Teflon (DuPont FEP 121-A). The total volume, including the connections to the mass spectrometer (MS) and to the pressure gauge (0.01–100 mTorr; 1 Torr corresponds to 1.333 hPa), is 120 cm^3 . The volume of the sample compartment is just 2.45 cm^3 which reduces artefacts caused by changes in the Knudsen reactor volume after the isolation plate is opened. The main compartment of the Knudsen reactor is coupled to the MS via a variable diameter escape orifice. In the present experiments a 3.5 mm diameter orifice was used. Before entering the MS, the molecular beam was modulated by a punched wheel chopper at 244 Hz, permitting phase-sensitive detection. The molecular beam was ionised with a cross-beam rhenium ion source, and ions were mass selected with a quadrupole analyser and detected with a secondary electron multiplier. The escape rate constants k_{esc} for the species involved were calculated from the mass and temperature dependent expression presented in a previous publica-

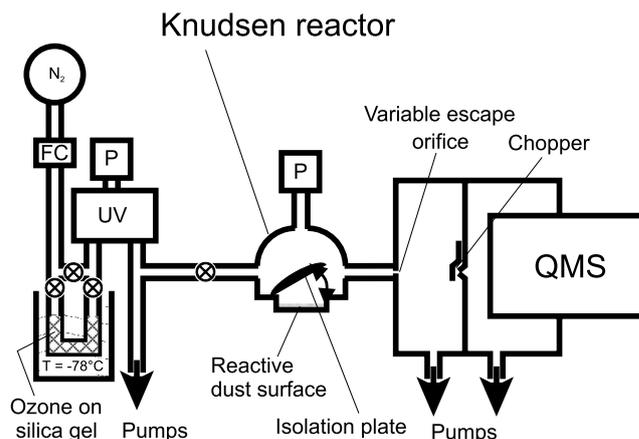


Fig. 1. Schematic diagram of the experimental set-up including Knudsen reactor, quadrupole mass spectrometer (QMS), pressure gauges (P), UV absorption facility (UV), and mixing line with flow controllers (FC). The pressure in the Knudsen reactor was generally $< 1 \text{ mTorr}$, the pressure in the mixing line about 5 Torr, and the pressure in the mass spectrometer chamber about 10^{-6} Torr .

tion (Hanisch and Crowley, 2001). They are listed in Table 1, together with other relevant Knudsen reactor parameters.

2.2 Reactant gas preparation

Ozone, generated with a commercial ozone generator and stored on silica gel in a U-tube at dry ice temperature, was transported to the Knudsen reactor in a variable nitrogen eluent flow, and its concentration was monitored directly by UV absorption at 254 nm over a 1 cm path length.

2.3 Dust sample characterisation and preparation

The Saharan dust used in these experiments originates from the Cape Verde Islands (SDCV). The composition of SDCV, as determined by energy dispersive X-ray spectroscopy, is given in Table 2. The SDCV samples were prepared by mixing between 2.3 and 96.4 mg of dust into a paste with ethanol or water and dispersed on polished $\alpha\text{-Al}_2\text{O}_3(11\bar{2}0)$ single crystals (surface area 1.0 cm^2 or 2.25 cm^2 ; MaTecK, Jülich, Germany), which were placed in the sample compartment and left under vacuum ($p \sim 2 \times 10^{-6} \text{ Torr}$) for 2 to 20 h. Some of the samples were additionally heated to $\approx 450 \text{ K}$ for 5 h under vacuum. When referring to sample masses, we always normalise to an area of 1 cm^2 in order to make measurements of uptake coefficients, using the two sample supports, comparable.

The density of single SDCV particles (averaged over an ensemble) was measured with a Helium pycnometer (Micro-metrics AccuPyc 1330). We refer to this as the “true density”. The bulk density of the substrate was not determined for each sample used to measure O_3 uptake, but derived in separate experiments in which larger amounts of dust were

Table 2. Composition of SDCV, as determined with energy dispersive X-ray spectroscopy

Compound	%
Na ₂ O	2.1
MgO	5.1
Al ₂ O ₃	17.6
SiO ₂	47.1
P ₂ O ₅	0.6
SO ₃	0.3
K ₂ O	2.5
CaO	5.0
TiO ₂	4.5
MnO	(0.3)
FeO	14.7

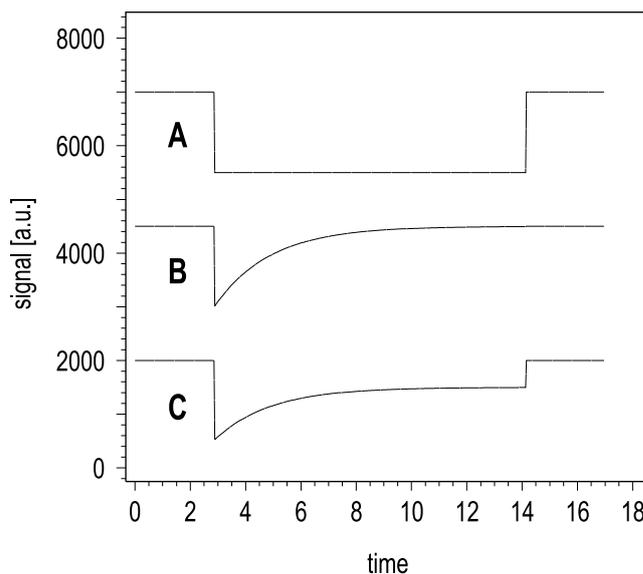
used (ca. 1 g), for which the sample volume could be precisely determined using a calibrated cylinder. Measurements of bulk density were frequently undertaken to investigate the reproducibility of the procedure, which was found to be better than $\pm 10\%$. For dust samples used in the uptake experiments (typically 5–50 mg) the sample height could not be determined in this way with sufficient precision, and was derived from the bulk density, and the geometry of the sample holder. The assumption inherent to this procedure is that the light samples have the same bulk density as the heavy ones. The average particle diameter was determined with a Palas Particle Counter Sizer 2010, and the BET surface areas were measured with a Quantachrome Autosorb 6B.

2.4 Measurement procedure and data analysis

Uptake coefficients, γ , were determined in continuous flow experiments at room temperature (296 K). The pressure, p , inside the Knudsen reactor was less than 1 mTorr, i.e. the experiments were performed in the molecular flow regime. The O₃ concentration inside the Knudsen reactor was systematically varied between $3.1 \times 10^{10} \text{ cm}^{-3}$ and $1.7 \times 10^{13} \text{ cm}^{-3}$. The corresponding O₃ flows through the Knudsen reactor into the MS were between $3.0 \times 10^{12} \text{ s}^{-1}$ and $1.7 \times 10^{15} \text{ s}^{-1}$ ($F_{\text{O}_3} = 97.28 \text{ cm}^3 \text{ s}^{-1} \times [\text{O}_3]$). O₃ was monitored by the mass spectrometer at $m/z = 48$ (O₃⁺) and O₂ at $m/z = 32$ (O₂⁺).

The uptake probability γ is defined as the ratio of the number of collisions with the surface that lead to removal from the gas phase to the total number of collisions with the surface and is given according to Benson and Spokes (1967):

$$\gamma = \frac{k_{uni}}{\omega} = \frac{k_{esc}}{\omega} \cdot \left(\frac{S_0}{S(t)} - 1 \right), \quad (1)$$

**Fig. 2.** Synthetic data: uptake without surface passivation (trace A); uptake with complete surface passivation (trace B); uptake with partial surface passivation (trace C). See text for details.

where k_{uni} is the pseudo-first-order rate constant, ω the collision frequency of a molecule with the reactive surface area of the sample, k_{esc} the escape rate constant, S_0 the MS signal of the reactant gas prior to raising the isolation plate, and $S(t)$ the signal at time t after raising the isolation plate.

3 Results and discussion

The Knudsen reactor technique is suited for the determination of uptake coefficients of trace gases adsorbed onto surfaces and for the observation of gas-phase products formed in heterogeneous reactions. The time dependence of the experimental uptake coefficient can take on several forms, which contain information about the nature of the gas-surface interaction. In Fig. 2, we display three synthetic data sets that describe the expected response of the measured trace gas concentration as a function of the exposure time for a trace gas interacting with a solid surface. (Traces A and C are shifted up- and downwards, respectively, relative to trace B.) In trace A, the uptake coefficient displays no dependence on time over the exposure period (3 min $< t < 14$ min). Such data sets may be obtained in irreversible uptake when sufficiently low trace-gas concentrations are used, that do not appreciably modify the composition of the surface or modify the concentration of a second surface reactant at time t , compared to time t_{open} . If higher trace gas concentrations are used, the time dependence of the uptake coefficient can take the form of trace B, which shows an initially large uptake coefficient that goes to zero at long exposure times. This can be explained by complete removal of reactive sites during an

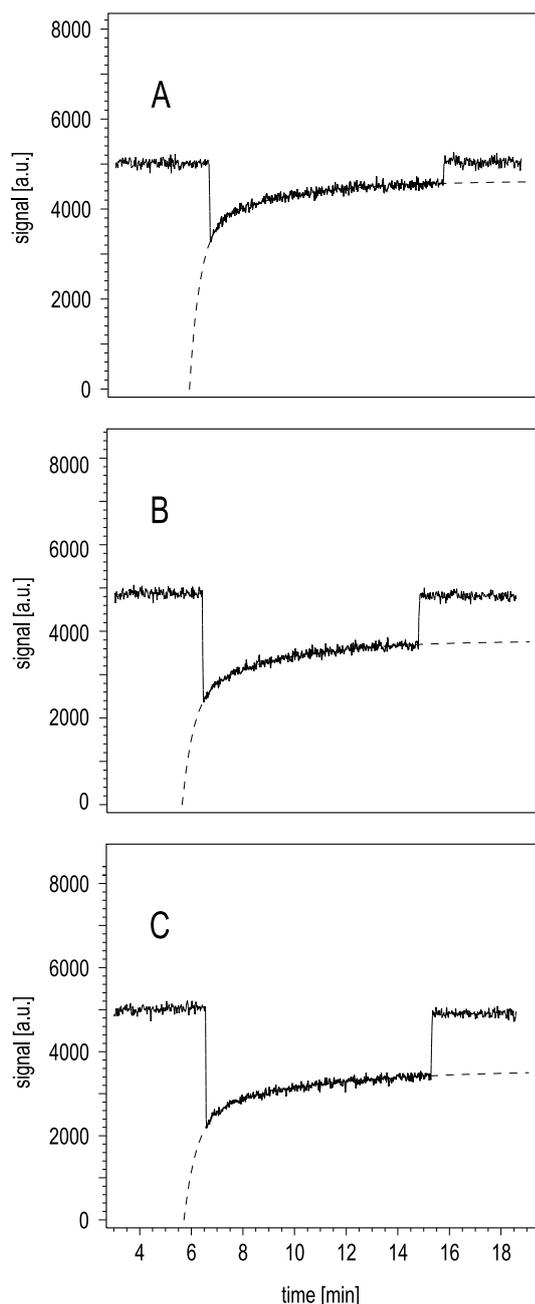


Fig. 3. Raw data showing the uptake of O_3 ($m/z = 48$; $[\text{O}_3] = 2.8 \times 10^{11} \text{ cm}^{-3}$) onto 2.3 mg/cm^2 (**A**), 7.6 mg/cm^2 (**B**), and 14.2 mg/cm^2 SDCV (**C**); the dashed lines correspond to modified bi-exponential fits that were used for the determination of $S(t_{\text{open}})$ and S_{∞} .

irreversible reactive uptake process, or by surface saturation during a reversible process at equilibrium. The time dependence will depend on the concentration of the trace gas and on the surface area of the bulk substrate available for reaction. Trace C displays the situation where an initially large uptake coefficient decreases over time to a constant, non-zero

value at longer exposure. This form of the time dependence may be encountered when, e.g. chemically or physically different sites are available for trace-gas uptake, one of which can support irreversible, catalytic uptake and the other can be de-activated on the experimental time scale. It may also be encountered when, during reactive uptake, passivation and re-activation of surface sites takes place on a similar time-scale.

For each type of data set, two distinct uptake coefficients have to be distinguished: the steady-state uptake coefficient, and the initial uptake coefficient. The initial uptake coefficient, γ_o , obtained immediately after opening the isolation plate at time t_{open} , is the same in each example with $\gamma_o = 0.5k_{\text{esc}}/\omega$. In contrast, the steady-state uptake coefficient, γ_{ss} , can be as large as γ_o (trace A) as low as zero (trace B) or any number between (trace C). The analysis of C-type profiles can be complicated by surface processes, which may involve diffusion into, e.g. a porous bulk substrate, and surface re-organisation and de- and reactivation. In addition, in trace types B and C the measured initial uptake coefficient is often observed to decrease with increasing trace gas concentration (due to rapid surface passivation on the time scale of data-acquisition to obtain γ_o) or when adsorption and desorption time scales are similar. Generally, the initial uptake coefficient can only be applied to model an uptake process in the atmosphere if the concentration of the respective trace gas is low enough (and the number of reactive sites is high enough) for surface passivation to be negligible over a period of several hours, i.e. over the lifetime of dust in the atmosphere.

In the present experiments the data was generally of the form given in trace C, and the uptake process is characterised by both an initial and a steady-state uptake coefficient. The use of atmospherically relevant O_3 concentrations was therefore an important consideration in this work, as uncertainties regarding extrapolation of results to the situation in the atmosphere can be reduced.

3.1 The uptake coefficient for O_3 onto SDCV

Most experiments were performed using samples with the dust being dispersed onto the support with ethanol. For a few samples water was used instead of ethanol; within the limit of uncertainty no difference in the uptake coefficients could be observed.

3.1.1 Dependence on sample mass and O_3 flow

Raw data showing the uptake of O_3 onto SDCV at three different sample masses (2.3 , 7.6 , and 14.2 mg/cm^2) are presented in Fig. 3. The MS signal at $m/z = 48$ corresponded to an O_3 concentration of $[\text{O}_3] = 2.8 \times 10^{11} \text{ cm}^{-3}$. When the isolation plate was open ($6.5 \text{ min} < t < 15.5 \text{ min}$), a clear reduction in signal intensity at $m/z = 48$ was detected. From the difference in signal intensity at $m/z = 48$ before and

after opening the isolation plate at t_{open} an initial uptake coefficient, γ_o^{geom} , can be calculated according to Eq. (1). The superscript “geom” signifies that the uptake coefficient was calculated using the geometric surface area A^{geom} of the sample. The three panels of Fig. 3 demonstrate that the amount of O_3 taken up by the dust sample for a given exposure period is dependent on the sample mass. For the experiments shown in Fig. 3 the following initial uptake coefficients have been determined: A (2.3 mg/cm^2): $\gamma_o^{\text{geom}} = 0.5 \times 10^{-2}$, B (7.6 mg/cm^2): $\gamma_o^{\text{geom}} = 1.0 \times 10^{-2}$, and C (14.2 mg/cm^2): $\gamma_o^{\text{geom}} = 1.3 \times 10^{-2}$. γ_o^{geom} clearly increases with increasing sample mass.

Similarly, a steady-state uptake coefficient $\gamma_{ss}^{\text{geom}}$ can be calculated from the asymptote S_∞ of a modified bi-exponential fit to the data during exposure:

$$S(t) = S_\infty - a_1 \exp(-k_1(t - t_{\text{open}})) - a_2 \exp(-k_2(t - t_{\text{open}})). \quad (2)$$

This expression has no physical basis, but allows us to extract precise values (statistical errors of about 1%) of S_∞ . We note that the difference between values of S_∞ derived by fitting compared to those obtained by visual inspection were about 10%. Similar to γ_o^{geom} , $\gamma_{ss}^{\text{geom}}$ increases with increasing sample mass (A: $\gamma_{ss}^{\text{geom}} = 0.9 \times 10^{-3}$, B: $\gamma_{ss}^{\text{geom}} = 3.1 \times 10^{-3}$, and C: $\gamma_{ss}^{\text{geom}} = 4.5 \times 10^{-3}$). At this O_3 concentration ($[\text{O}_3] = 2.8 \times 10^{11} \text{ cm}^{-3}$), initial uptake coefficients are bigger than steady-state uptake coefficients by a factor 3–5.

The phenomenon of geometric uptake coefficients being dependent on sample mass is frequently observed for the interaction of trace gases with porous bulk substrates and is due to diffusion of molecules into interstitial space. This results in an overestimation of the uptake coefficient if A^{geom} is used to calculate it. Keyser and co-workers have developed a model for ice surfaces (Keyser and Leu, 1991, 1993) which in principle can also be applied to granular surfaces (e.g. Timonen et al., 1994; Leu et al., 1995). This model predicts a linear dependence of the uptake coefficient on the sample mass if the sample height is much less than the diffusion depth of the gas molecules into the bulk sample. The dependence becomes weaker as the thickness of the bulk sample becomes larger than the diffusion depth of the gas molecules, and eventually reaches a plateau. This model can be used to extract the “true” uptake coefficient from the one based on the geometric surface area. Once corrected for pore diffusion, the uptake coefficient γ^{pd} can be considerably smaller than that based on the geometrical surface area, γ^{geom} . The two uptake coefficients are related to each other by:

$$\gamma^{\text{geom}} = \gamma^{pd} \rho_b A^{\text{BET}} \bar{d} \left(\frac{1}{2} + \eta \left(\frac{h}{\bar{d}} - \frac{1}{2} \right) \right), \quad (3)$$

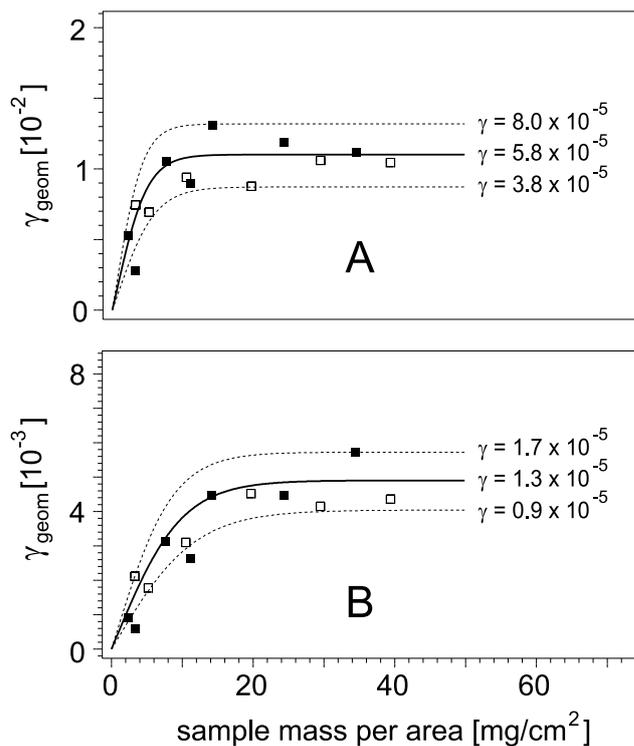


Fig. 4. Plot of geometric uptake coefficients of O_3 ($[\text{O}_3] = 2.8 \times 10^{11} \text{ cm}^{-3}$) on SDCV versus normalised sample mass: (A) initial uptake coefficients γ_o , (B) steady-state uptake coefficients γ_{ss} . Filled symbols represent experiments with ethanol dispersed samples, open symbols experiments with water dispersed samples. The data have been fitted by the pore diffusion model (central solid lines; the dashed lines give the range of uncertainty).

where η is the “effectiveness” factor, $\eta = \frac{\tan \phi}{\phi}$, and ϕ is the Thiele modulus whereby:

$$\phi = \left(\frac{h}{\bar{d}} - \frac{1}{2} \right) \left(\frac{3\rho_b}{2(\rho_t - \rho_b)} \right) \sqrt{3\tau\gamma^{pd}}. \quad (4)$$

The input parameters for the calculation of the pore diffusion-corrected uptake coefficient γ^{pd} of O_3 onto SDCV are: the geometric uptake coefficient γ^{geom} , the total height of the sample h , the average grain size of the particles ($\bar{d} = 0.9 \mu\text{m}$), the true density $\rho_t (= 2.7 \text{ g/cm}^3)$, the bulk density $\rho_b (= 1.2 \text{ g/cm}^3)$, the specific BET surface area $A^{\text{BET}} (= 39.6 \text{ m}^2/\text{g})$ and the tortuosity factor τ , which may be regarded as a measure of hindrance to diffusive mass transfer into the pores of the sample, and which will depend on physical characteristics of both the bulk substrate and the gaseous species. Values of τ are usually empirically determined by measuring the variation of the uptake coefficient with sample mass. The sample heights, normalised to sample areas of 1 cm^2 , were calculated from the sample mass m , the bulk density ρ_b and the surface area of the sample holder.

Figure 4 shows the results for γ_o^{geom} (panel A) and $\gamma_{ss}^{\text{geom}}$ (panel B) for the complete set of experiments at $[\text{O}_3] =$

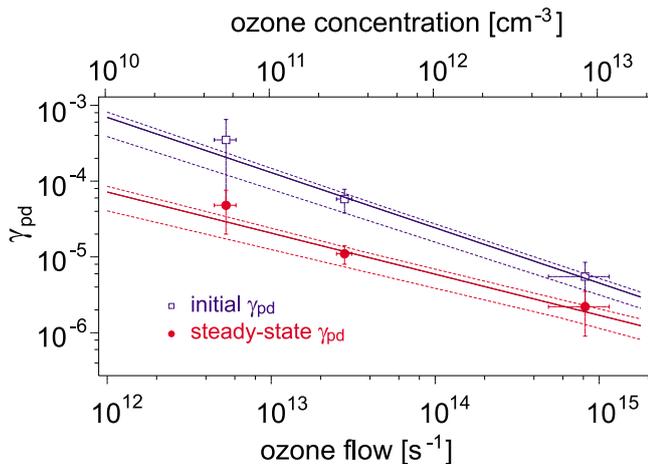


Fig. 5. Plot of pore diffusion-corrected initial and steady-state uptake coefficients of O_3 on SDCV versus O_3 concentration and flow, respectively. The error bars denote fluctuations in the O_3 concentration and the upper and lower limits of the uptake coefficients as obtained from the pore-diffusion model, respectively. The dashed lines give the 1σ -deviation from the fits.

$2.8 \times 10^{11} \text{ cm}^{-3}$ (13 experiments, sample mass 2.3 to 39.4 mg/cm^2). The data can be reproduced with the pore diffusion model using a tortuosity factor $\tau = 1$ to yield $\gamma_o^{pd} = (5.8^{+2.2}_{-2.0}) \times 10^{-5}$ and $\gamma_{ss}^{pd} = (1.3 \pm 0.4) \times 10^{-5}$ (solid fit lines). The dashed lines give the upper and lower limits, respectively, within which most of the data points lie.

A further 14 experiments were carried out at O_3 concentrations of $[\text{O}_3] = (8.4 \pm 3.4) \times 10^{12} \text{ cm}^{-3}$ and with varying sample mass. The results for the uptake coefficients are summarised in Table 3. The measured initial and steady-state uptake coefficients were fit according to Eqs. (3)–(4), giving as final results $\gamma_o^{pd} = (5.5^{+4.0}_{-3.0}) \times 10^{-6}$ and $\gamma_{ss}^{pd} = (2.2^{+1.4}_{-1.2}) \times 10^{-6}$.

Similarly, 15 experiments were carried out at O_3 concentrations of $[\text{O}_3] = (5.4 \pm 0.8) \times 10^{10} \text{ cm}^{-3}$ and with varying sample mass. The results for the uptake coefficients are summarised in Table 4. The fits according to Eqs. (3)–(4) yielded $\gamma_o^{pd} = (3.5^{+3.5}_{-2.5}) \times 10^{-4}$ and $\gamma_{ss}^{pd} = (4.8^{+3.2}_{-2.4}) \times 10^{-5}$. In all cases, $\tau = 1$ was used.

These results show that both $\gamma_{ss}^{\text{geom}}$ and γ_{ss}^{pd} are smaller than γ_o^{geom} and γ_o^{pd} , by factors 3–7, respectively, with the biggest difference occurring for the lowest O_3 flows. In Fig. 5, the pore diffusion corrected uptake coefficients (both the initial ones (open squares) and the steady-state ones (solid circles)) are plotted versus O_3 concentration and flow. The solid lines in Fig. 5 are exponential functions that describe an empirical expression for the dependence of γ_o^{pd} and γ_{ss}^{pd} on $[\text{O}_3]$: $\gamma^{pd} = a[\text{O}_3]^{-b}$, where $[\text{O}_3]$ is in cm^{-3} . For the initial uptake coefficient we derive $a = 1.48 \times 10^4$ and $b = 0.73$, for the steady-state uptake coefficient $a = 19.2$

Table 3. Uptake experiments with O_3 onto SDCV at $[\text{O}_3] = (8.4 \pm 3.4) \times 10^{12} \text{ cm}^{-3}$

$[\text{O}_3]$ (cm^{-3})	mass (mg/cm^2)	$\gamma_o/10^{-3}$	$\gamma_{ss}/10^{-4}$
9.0×10^{12}	4.6	1.3	0.9
1.1×10^{13}	5.0	6.9	0.4
1.1×10^{13}	10.0	1.4	0.4
9.2×10^{12}	10.7	2.4	1.7
1.1×10^{13}	15.2	2.7	1.1
4.6×10^{12}	17.9	1.6	0.7
1.2×10^{13}	25.0	2.0	1.4
6.9×10^{12}	26.1	3.9	1.6
1.0×10^{13}	30.3	1.7	1.2
6.1×10^{12}	33.4	2.4	1.4
1.1×10^{13}	40.1	2.9	2.0
9.0×10^{12}	42.0	4.3	2.2
1.1×10^{13}	45.6	2.6	1.4
9.4×10^{12}	51.1	3.2	1.2

$$\gamma_o^{pd} = (5.5^{+4.0}_{-3.0}) \times 10^{-6}$$

$$\gamma_{ss}^{pd} = (2.2^{+1.4}_{-1.2}) \times 10^{-6}$$

Table 4. Uptake experiments with O_3 onto SDCV at $[\text{O}_3] = (5.4 \pm 0.8) \times 10^{10} \text{ cm}^{-3}$

$[\text{O}_3]$ (cm^{-3})	mass (mg/cm^2)	$\gamma_o/10^{-2}$	$\gamma_{ss}/10^{-3}$
5.4×10^{10}	3.2	1.1	4.6
5.0×10^{10}	3.3	1.4	1.9
6.1×10^{10}	5.1	1.3	4.1
4.7×10^{10}	6.3	2.5	6.5
5.5×10^{10}	9.8	3.3	7.6
4.7×10^{10}	12.3	5.0	9.2
5.2×10^{10}	14.5	1.7	5.0
5.3×10^{10}	14.9	2.9	7.7
7.4×10^{10}	21.6	2.8	8.0
5.1×10^{10}	24.7	2.7	6.9
3.9×10^{10}	30.3	1.1	6.0
5.1×10^{10}	30.6	5.4	10.0
5.4×10^{10}	34.9	2.2	6.3
3.3×10^{10}	40.6	2.2	4.5
5.9×10^{10}	41.1	4.1	8.9

$$\gamma_o^{pd} = (3.5^{+3.5}_{-2.5}) \times 10^{-4}$$

$$\gamma_{ss}^{pd} = (4.8^{+3.2}_{-2.4}) \times 10^{-5}$$

and $b = 0.54$. The exponential fits are weighted by the estimated error of γ .

A possible cause of the observed reduction in uptake coefficients as the O_3 concentration was increased is rapid passivation of the surface. In order to test this, uptake of O_3

onto 40.6 mg/cm^2 SDCV at two different O_3 concentrations was investigated, as shown in Fig. 6: At $t = 2.5 \text{ min}$ an O_3 concentration of $[\text{O}_3] = 3.6 \times 10^{10} \text{ cm}^{-3}$ was established but not exposed to the dust surface. When the isolation plate was opened at $t = 13 \text{ min}$, O_3 was taken up by SDCV ($\gamma^{\text{geom}} = 2.2 \times 10^{-2}$). The partial recovery of the MS signal indicated partial surface passivation, resulting in a value for γ^{geom} of 6.3×10^{-3} at 24 min, shortly before the sample was isolated again. At $t = 35.7 \text{ min}$ the O_3 concentration was increased to $[\text{O}_3] = 4.7 \times 10^{11} \text{ cm}^{-3}$ and at $44.5 \text{ min} < t < 50.8 \text{ min}$, the isolation plate was again lifted leading to uptake of O_3 . This time an uptake coefficient was observed that decreased from $\gamma^{\text{geom}} = 5.0 \times 10^{-3}$ ($t = 44.5 \text{ min}$) to 3.5×10^{-3} ($t = 50.8 \text{ min}$). Finally, the O_3 concentration was lowered to $3.6 \times 10^{10} \text{ cm}^{-3}$ at $t = 54.7 \text{ min}$ and the uptake of ozone was found to be slightly enhanced with respect to the previous exposure period, with γ^{geom} decreasing from 5.6×10^{-3} ($t = 59 \text{ min}$) to 4.6×10^{-3} ($t = 63 \text{ min}$).

From the experiment shown in Fig. 6 it can be seen that, for a given sample mass, γ^{geom} depends not only on the degree of passivation of the sample but also directly on the O_3 concentration. This explains the observation that the uptake coefficient at $59 \text{ min} < t < 63 \text{ min}$ was larger than that at $t = 50.8 \text{ min}$. The enhanced availability of reaction sites at lower O_3 concentrations (evidenced by the increase in γ) cannot be explained by reversible uptake of O_3 leading to passivation, as no desorption of O_3 was observed after shutting off the O_3 flow. A potential explanation for the apparent enhanced reactivity at low ozone concentrations is related to the blocking of reactive sites by ozone molecules temporarily occupying neighbouring non-reactive sites. This is apparent in Fig. 6, where the reactivity is first lowered at high ozone concentrations, but increases when [ozone] is lowered again for the same dust sample. Surface sensitive studies could clarify this. We note that a comparable ozone concentration dependence for uptake to carbonaceous surfaces has been observed (Stephens et al., 1986).

3.1.2 The influence of sample heating on the uptake coefficient

Another series of experiments was conducted with SDCV samples, heated prior to the experiment, at $[\text{O}_3] \sim 8 \times 10^{12} \text{ cm}^{-3}$ and with varying sample mass. Geometric uptake coefficients were higher than for unheated samples by about a factor of two. The data could be fitted with the pore diffusion model using $\tau = 1$. The pore diffusion corrected uptake coefficient for heated SDCV ($\gamma_o^{\text{pd}} = (1.25 \pm 0.45) \times 10^{-5}$) was also higher than the one for unheated SDCV ($\gamma_o^{\text{pd}} = (5.5_{-3.0}^{+4.0}) \times 10^{-6}$).

3.1.3 Comparison with literature

O_3 uptake on Saharan sand has been investigated using a fluidised-bed reactor (Alebic-Juretic et al., 1992). Although

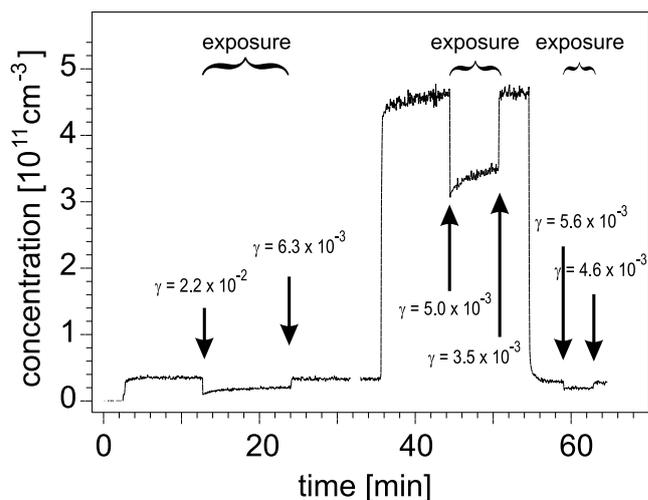


Fig. 6. Raw data showing the uptake of O_3 ($m/z = 48$) onto 40.6 mg/cm^2 SDCV; the O_3 concentration has been changed from $3.6 \times 10^{10} \text{ cm}^{-3}$ to $4.7 \times 10^{11} \text{ cm}^{-3}$ (at $t = 35.7 \text{ min}$) and back again to $3.6 \times 10^{10} \text{ cm}^{-3}$ (at $t = 54.7 \text{ min}$). “Exposure” indicates periods in which contact between O_3 and dust took place.

uptake coefficients were not derived they can be estimated from the data presented, according to the formula:

$$-\frac{d}{dt}[\text{O}_3] = \frac{\bar{c}}{4} \gamma A_{\text{dust}}[\text{O}_3] \quad (5)$$

A_{dust} is the surface area density of the substrate and equals the product of BET surface area of the substrate (cm^2/g) and sample mass per reactor volume (g/cm^3). For Saharan sand the signal reduction presented in that paper corresponds to an initial uptake coefficient of $\gamma_o = 2.3 \times 10^{-7}$ at $[\text{O}_3] = 2.5 \times 10^{12} \text{ cm}^{-3}$ (100 ppbv). This is lower than the value extrapolated from our data by about one order of magnitude, which may be related to overestimation of the available surface area if the O_3 molecules only have a limited diffusion depth into the bulk. In a similar manner, initial uptake coefficients for Al_2O_3 ($\gamma_o = 6.6 \times 10^{-9}$) and calcite ($\gamma_o = 4.3 \times 10^{-7}$) can be calculated from the data given in that study.

An earlier study on the decomposition of O_3 on $\gamma\text{-Al}_2\text{O}_3$ at room temperature (Klimovskii et al., 1983) reports a decomposition efficiency of O_3 of 10^{-4} ($[\text{O}_3] = 1 \times 10^{13}$ to $3 \times 10^{15} \text{ cm}^{-3}$), though it is unclear whether geometric or BET surface areas were used to derive this value. Uptake coefficients for the interaction of O_3 with various types of Al_2O_3 have also been obtained from a flow-tube study at 213–473 K (Hanning-Lee et al., 1996). These authors derived pore-diffusion corrected uptake coefficients that were independent of O_3 concentration (5×10^{15} to $2 \times 10^{17} \text{ cm}^{-3}$) and varied, depending on temperature, between 2×10^{-11} and 3×10^{-9} .

A very recent Knudsen reactor study determined $\gamma_o = (6 \pm 3) \times 10^{-5}$ as an upper limit for O_3 uptake on

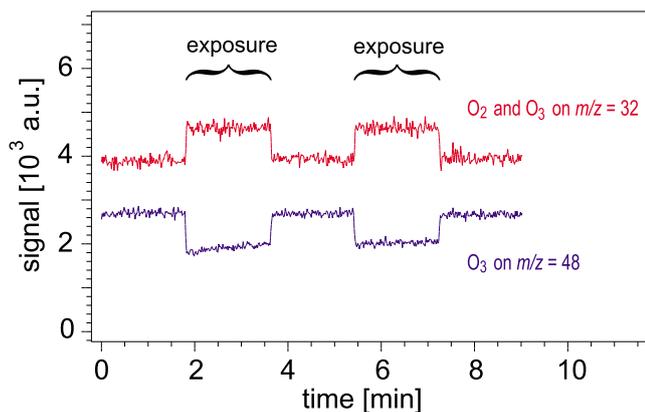


Fig. 7. Raw data showing the uptake of O_3 ($m/z = 48$; $[\text{O}_3] = 6.2 \times 10^{12} \text{ cm}^{-3}$) onto 33.4 mg/cm^2 SDCV, associated with release of O_2 ($m/z = 32$). “Exposure” indicates periods in which contact between O_3 and dust took place.

ground Saharan sand at $[\text{O}_3] = 1.9 \times 10^{11} \text{ cm}^{-3}$ (Michel et al., 2002). This is in accord with the result calculated from our empirical expression for the initial uptake coefficient in Sect. 3.1.1 ($\gamma_o^{pd} = (8.6 \pm 2.0) \times 10^{-5}$). Although Michel et al. (2002) observed that the uptake coefficient decreased considerably with time, no steady-state uptake coefficient was determined. Other initial uptake coefficients determined by Michel et al. (2002) for $\alpha\text{-Al}_2\text{O}_3$, $\alpha\text{-Fe}_2\text{O}_3$, SiO_2 , and China loess were in the range 10^{-5} to 10^{-4} . In contrast to our results, no variation in the initial uptake coefficient was observed as the O_3 concentration was varied between 10^{11} and 10^{12} cm^{-3} .

Finally, measurements of O_3 deposition velocities (v_{dep}) have been performed on various surfaces, including kaolin, sand and CaCO_3 (Garland, 1974). Using these data and the formula $\gamma = 4v_{dep}/\bar{c}$, Dentener et al. (1996) calculated uptake coefficients in the range 10^{-4} to 10^{-5} . This estimate falls within the range of our results for O_3 concentrations lower than about $4 \times 10^{11} \text{ cm}^{-3}$ (corresponding to 16 ppbv at STP) if the steady-state uptake coefficients are used.

Our finding that O_3 uptake on heated SDCV samples is greater than on unheated samples is consistent with the observation that O_3 is much more efficiently destroyed on dry soil than on moist soil (Aldaz, 1969). The same has been observed for O_3 decomposition on $\gamma\text{-Al}_2\text{O}_3$ (Hanning-Lee et al., 1996), and on a $\text{Pt}/\gamma\text{-Al}_2\text{O}_3$ catalyst at 50–90% RH (Tsai et al., 1998). The reduced uptake can be explained by occupation of reactive sites by H_2O molecules or by the complete blocking of pores (Galbally and Roy, 1980). Note that the heated samples are considered less representative of the situation in the atmosphere in which relative humidities are generally greater than $\sim 30\%$.

3.2 O_3 decomposition and O_2 production

3.2.1 Heated and unheated dust samples

Raw data showing the uptake of O_3 ($[\text{O}_3] = 6.3 \times 10^{12} \text{ cm}^{-3}$) onto 33.4 mg/cm^2 of heated SDCV are presented in Fig. 7. When the isolation plate was open ($1.8 \text{ min} < t < 3.6 \text{ min}$, and $5.4 \text{ min} < t < 7.2 \text{ min}$), both uptake of O_3 (reduction in signal) and an increase of the signal at $m/z = 32$ are visible. Clearly, O_3 is destroyed on the dust surface and O_2 is produced. The $m/z = 32$ signal comprised contributions both from O_3 (ion fragment) and O_2 . Hence, for calculating the stoichiometry of the O_3 to O_2 conversion, the fragment pattern of O_3 on $m/z = 48$ and $m/z = 32$ was precisely determined and used to remove the contribution of O_3 to the signal at $m/z = 32$. The resultant signal, due to O_2 only, was converted to a flow by comparison to calibration signals.

For the analysis it was important to ensure that no significant O_2 impurity was present in the O_3 flow. This was achieved by comparing the sum of the O_3 and N_2 partial pressures, as determined by the MS, with the total Knudsen reactor pressure (capacitance manometer). (Recall that O_3 is mixed into an N_2 flow.) These pressures agreed to better than 2%, allowing us to place a conservative upper limit of $\approx 5\%$ to the O_2 impurity in the ozone. This O_2 impurity represents the main contributor to the error of the O_3 to O_2 conversion stoichiometry.

For the catalytic interaction of O_3 with surfaces a mechanism has been proposed (Golodets, 1983) in which a terminal O atom of O_3 binds to a surface site and results in dissociation of O_3 into O_2 and O, leaving the O atom at the surface. The stoichiometry of this step is unity, i.e. one gas-phase O_3 molecule reacts to form one O_2 molecule. Surface bound O can further react with O_3 to form two O_2 molecules per O_3 molecule adsorbed, or, if temperatures are high enough, two O atoms can migrate over the surface, meet and recombine to form an O_2 molecule. In both cases, the net result is three O_2 molecules formed from two O_3 molecules.

In the present experiments using heated dust samples, the ratio of O_2 produced to O_3 taken up at steady state, i.e. after several minutes of exposure when the O_3 signal remained constant, was found to be 1.30 ± 0.05 . The difference to the theoretical stoichiometry of 1.5 (3 O_2 molecules released per 2 O_3 molecules taken up) can be explained if it is assumed that some O atoms remain on the surface after contact of O_3 with the surface and do not form molecular oxygen that desorbs. At the beginning of the sample exposure the O_3 to O_2 conversion stoichiometry did change: The conversion efficiency of O_3 to O_2 at short exposure times was found to be just 1.2, indicating an induction period before quasi-catalytic O_3 to O_2 conversion starts. In the limit of zero exposure to O_3 the stoichiometry cannot be greater than unity (i.e. the first O_3 molecule to be taken up cannot result in release of more than one O_2). Only with longer exposure time there is sufficient surface bound O which can react with a further O_3

molecule to increase the O₂ yield. Importantly, for experiments carried out using *unheated* dust samples the O₃ to O₂ conversion stoichiometry at steady-state uptake was found to be 1.0, which means that in the presence of water not only the O₃ uptake coefficient but also the O₃ to O₂ conversion stoichiometry is reduced.

3.2.2 The uptake mechanism

So far, the hypothesis of Golodets (1983) has only indirectly and qualitatively been tested: The formation of O atoms after adsorption of O₃ onto TiO₂ at 77 K has been verified by formation of CO₂ after addition of CO to the surface (Bulanin et al., 1995b). Also the release of O₂ has been proven only indirectly, by a pressure increase during the O₃ decomposition process (Hanning-Lee et al., 1996; Thomas et al., 1997), and qualitatively by the assignment of certain bands in Raman spectra to gaseous O₂ (Li et al., 1998). Our determination of an O₃ to O₂ conversion stoichiometry of 1.3 is, to our knowledge, the first quantitative proof that Golodets' hypothesis is at least partly correct. Further, we can rule out that the O₃ to O₂ conversion follows a Langmuir-Hinshelwood mechanism (simultaneous adsorption of two O₃ molecules at one reaction site) because such a reaction should be quadratic in [O₃], which, from Fig. 5, is clearly not the case. Therefore, O₃ to O₂ conversion follows an Eley-Rideal mechanism as proposed by Golodets (1983) and Li et al. (1998). Below, we explore ways to understand why not all O₃ is catalytically converted to O₂ and why the conversion stoichiometry is not the same for heated and unheated dust samples.

An FT-IR study (Bulanin et al., 1995a) investigated the uptake of isotopically labelled O₃ onto several mineral oxides at 77 K and verified that O₃ is adsorbed to the surface with one of its terminal O atoms. According to another FT-IR study of the same group on the interaction between O₃ and a partially hydrated TiO₂ surface (Bulanin et al., 1995b), at least three different types of surface sites for O₃ adsorption can be distinguished: (I) surface sites where O₃ is weakly bound to hydroxyl groups or by physisorption; (II) surface sites with weak Lewis acid character (unsaturated Ti^{IV} ions) where O₃ is chemisorbed but remains intact with distorted geometry; and (III) strong Lewis acid sites where adsorbed O₃ molecules are sufficiently distorted that they dissociate into O₂ and O. O₃ adsorption to surface sites type I is completely reversible, as was shown for O₃ adsorption onto partially hydrated SiO₂ (Bulanin et al., 1994). In the present experiments, if reversible O₃ uptake to OH groups (surface sites type I) had played a role, O₃ desorption after O₃ uptake should have been observable, which was not the case. Therefore, we conclude that at room temperature surface sites type I play a minor role in the uptake process.

Surface sites type II are a weak form of surface sites type III, with the strength and the number of Lewis acid sites increasing with increasing dehydration of the surface (Bulanin et al., 1995b). As type III sites are responsible for O₃ destruc-

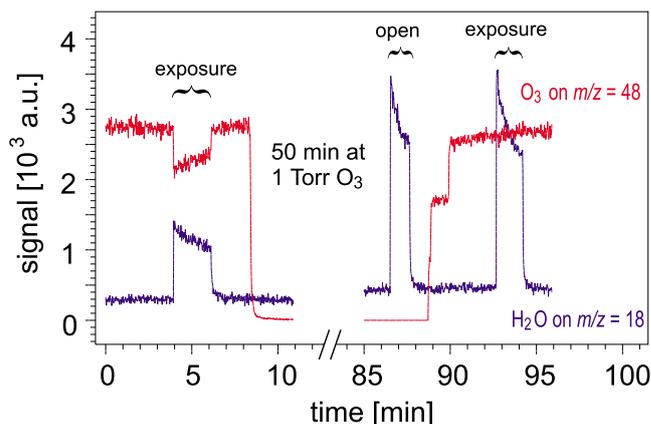


Fig. 8. Raw data showing the uptake of O₃ ($m/z = 48$; $[O_3] = 3.9 \times 10^{12} \text{ cm}^{-3}$) onto 16.4 mg/cm^2 SDCV before and after a 50 min exposure of the sample to 1 Torr of O₃. While O₃ uptake ceases after the exposure, water mobilisation ($m/z = 18$) is almost tripled.

tion, dehydration of the surface, i.e. by heating and evacuation should result in higher uptake coefficients and higher O₃ to O₂ conversion efficiencies, as observed in the present study.

Evidence for the interaction of O₃ with surface hydroxyl groups was obtained in the present work whereby the release of H₂O from samples exposed to O₃ showed a strong, positive dependence on [O₃]. The formation of H₂O may be attributed to exchange of hydroxyl with oxygen species at the surface, and subsequent recombination to form water. This is exemplified in Fig. 8: The amount of water released from an 16.4 mg/cm^2 SDCV sample and detected by the MS upon opening the isolation plate is almost tripled after a 50 min exposure of the sample to 1 Torr of O₃.

O₃ decomposition on strong Lewis acid sites may take place as suggested by Golodets (1983). However, the observation of an adsorbed peroxy species after uptake of O₃ to a MnO₂ surface has led to the formulation of a slightly modified reaction scheme (Li et al., 1998) in which the reaction of O₃ with an adsorbed O atom does not result in the immediate desorption of two O₂ molecules but only of one O₂ molecule, the other one remaining adsorbed as a peroxy species and desorbing with a slower rate constant.

3.3 Passivation of O₃ uptake

Our observations indicate that the uptake of O₃ is time dependent and decreases with increased exposure time due to surface passivation. The fact that the dust surface can be passivated with respect to O₃ uptake is related to the finding that the O₃ to O₂ conversion stoichiometry was smaller than 1.5. Catalytic O₃ to O₂ conversion with a stoichiometry of 1.5 would imply that no surface sites are consumed or passivated during the uptake process. A stoichiometry of 1.3 for heated dust samples and of 1.0 for unheated dust samples implies

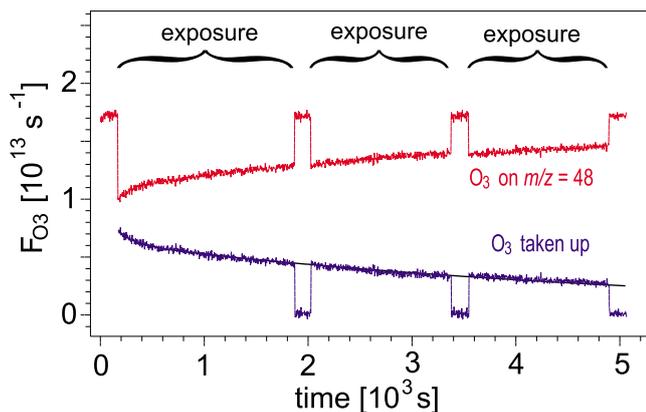


Fig. 9. Raw data showing the uptake of O_3 ($m/z = 48$) onto 17.6 mg/cm^2 SDCV; the O_3 concentration was $1.8 \times 10^{13} \text{ cm}^{-3}$ (upper curve). The lower curve shows the rate of O_3 destroyed by the dust surface. The data could be fitted with a bi-exponential function.

that O atoms stemming from the O_3 molecules must be lost to the surface.

In order to investigate passivation effects in detail, an experiment using a high O_3 concentration ($1.8 \times 10^{13} \text{ cm}^{-3}$, ~ 730 ppbv at STP) and 17.6 mg/cm^2 sample was carried out over an extended period of 1.3 h. The raw data from this experiment are shown in Fig. 9 (upper curve). The (geometric) uptake coefficient decreased from an initial value of 3.3×10^{-3} to 0.9×10^{-3} after 1.3 h. The number of molecules taken up by the surface could be fit by a bi-exponential function (Fig. 9, lower curve), although it was not possible to determine whether the uptake tends to zero or not at long exposure times. Assuming that the uptake indeed tends to zero, the total number of O_3 molecules destroyed by the surface can be estimated as $2.1 \times 10^{14} \text{ cm}^{-2}$. Longer exposure times could not be performed due to experimental limitations. Instead, another experiment was conducted with a similar sample mass, but with a passivation phase in which an O_3 concentration of ≈ 1 Torr ($\approx 3 \times 10^{16} \text{ cm}^{-3}$) was introduced into the reactor. The results of this experiment are depicted in Fig. 8. Prior to the passivation phase, an uptake coefficient $\gamma_o^{\text{geom}} = 3.0 \times 10^{-3}$ was determined as usual.

Following the passivation phase no O_3 uptake could be detected ($\gamma^{\text{geom}} < 1 \times 10^{-4}$) (i.e. no change in $m/z = 48$ at $t = 92.7$ min). Following evacuation at $\sim 2 \times 10^{-6}$ Torr overnight, the sample had partially recovered and a value of $\gamma_o^{\text{geom}} = 1.5 \times 10^{-3}$ was obtained indicating that reactivation processes have partly restored the sample reactivity overnight.

Complete passivation of the reactivity of Saharan sand was also observed in the study of Alebic-Juretic et al. (1992) who found it to be slower than passivation of calcite but much faster than passivation of Al_2O_3 . This can be explained by the facts that Saharan dust is a mixture of several mineral

components (Table 2), and that Lewis acid site strength decreases in the order $Al_2O_3 > TiO_2 > SiO_2 > MgO$ (Bulanin et al., 1995a; Thomas et al., 1997).

The presence of a peroxy species that is formed by reaction of O_3 with a surface-adsorbed O atom, and which slowly decomposes and then desorbs from the surface as molecular oxygen (Li et al., 1998) would be a possible explanation for passivation if this sequence was slow enough to block reactive sites. A further explanation would be the occupation of reactive sites by atomic oxygen followed by very slow recombination on the surface and subsequent desorption of O_2 . A detailed investigation of the mechanism of uptake and passivation requires application of surface sensitive techniques.

3.4 O_3 uptake onto other dusts

A few experiments were carried out at O_3 concentrations of $[O_3] \sim 6 \times 10^{12} \text{ cm}^{-3}$ and using “Arizona Test Dust”, Chinese dust from the Taklamakan desert, and the clay minerals kaolinite, illite, Ca-montmorillonite and palygorskite. Only initial uptake coefficients were determined, and no pore-diffusion corrected uptake coefficients can be given because the mass dependence of the geometric uptake coefficient was not investigated. However, the experiments were performed at high sample masses where no further variation of γ^{geom} with increasing sample mass is expected and can thus, to a first approximation, be compared to the SDCV experiments.

For all substrates the uptake coefficients were considerably lower when unheated samples were used. For unheated kaolinite and illite, γ^{geom} was near to or below the detection limit (1×10^{-4}). For Ca-montmorillonite no uptake was detected on an unheated sample ($\gamma^{\text{geom}} < 1 \times 10^{-4}$) while on a heated sample $\gamma_o^{\text{geom}} = 3.2 \times 10^{-2}$ was found. For a heated palygorskite sample $\gamma_o^{\text{geom}} = 2.0 \times 10^{-2}$ was determined. These results can be compared to the results for heated SDCV at $[O_3] \sim 8 \times 10^{12} \text{ cm}^{-3}$; they are higher than the results for heated SDCV by a factor of five. Interestingly, for an unheated Ca-montmorillonite sample which was prepared with ethanol $\gamma_o^{\text{geom}} = 1.8 \times 10^{-2}$ was measured. This is in contrast to the finding that uptake onto SDCV is not sensitive to the use of ethanol instead of water.

Uptake coefficients for unheated Chinese dust and “Arizona Test Dust” were $\gamma_o^{\text{geom}} = 3 \times 10^{-3}$ and $\gamma_o^{\text{geom}} = 2 \times 10^{-3}$, respectively. They were in the same range as γ_o^{geom} for unheated SDCV (see Table 3).

3.5 Atmospheric implications

As pointed out by Dentener et al. (1996), the global effect of dust on O_3 concentrations should be negligible if the uptake coefficient is $\gamma = 10^{-5}$ and lower. The pore diffusion corrected uptake coefficient determined in this work under steady-state conditions, γ_{ss}^{pd} , for atmospheric O_3 concentrations is $(7 \pm 3) \times 10^{-6}$, which is at the lower boundary of uptake coefficients used in modelling studies. In dust

plumes particle number densities are more than two orders of magnitude higher than the background level. Taking an aerosol surface area density of $A = 1.5 \times 10^{-6} \text{ cm}^2 \text{ cm}^{-3}$ for a dust plume (de Reus et al., 2000) and $\gamma = 10^{-5}$, the removal rate of O_3 with respect to processing by dust is $k_{\text{dust}} = 1.4 \times 10^{-7} \text{ s}^{-1}$ ($k_{\text{dust}} = \gamma \bar{c} A / 4$). This has to be compared to other loss processes of O_3 : photolysis with subsequent reaction of $\text{O}(^1\text{D})$ with H_2O , reaction of O_3 with HO_2 and reaction of O_3 with OH (Crutzen et al., 1999). Ozone loss due to these processes is in the same order of magnitude and only slightly higher than O_3 loss by reaction on dust. Since the photochemical gas-phase loss processes are active only during the day, O_3 loss by reaction on dust could be most important during night.

The preceding arguments hold if the destruction of O_3 on the dust surface is catalytic without surface passivation. If, however, the surface of dust particles in the atmosphere were permanently passivated with respect to the uptake of O_3 , the quantification of the O_3 uptake capacity of dust is important. In Sect. 3.3, a capacity of 2.1×10^{14} O_3 molecules destroyed per cm^2 of dust was calculated for SDCV. This is too low for mineral aerosol to have a noticeable effect on atmospheric O_3 concentrations because, even in plumes, mineral aerosol surface areas are of the order of $10^{-6} \text{ cm}^2 \text{ cm}^{-3}$. The measured bulk capacity also allows us to calculate the capacity of a single dust particle of 1 micron diameter to be approximately 1×10^7 molecules of O_3 . Combining the measured uptake coefficient of ca. 1×10^{-5} with an ozone concentration of 40 ppb (ca. $1 \times 10^{12} \text{ O}_3 / \text{cm}^3$) and a calculated collision frequency we can derive an approximate time for passivation of 100 s. However, several observations argue against complete mineral aerosol surface passivation. Firstly, in the experiment described in Sect. 3.3 it was possible to partly restore the sample reactivity. Even if the re-activation processes are presently unknown, they should also be operating in the atmosphere, and may well be more efficient than in the dry, chemically clean Knudsen reactor environment. Note that deposition velocity measurements have shown, e.g. that exposure to SO_2 rejuvenates the capacity of the surface for reaction with ozone (Garland, 1974). Secondly, the dust used in our experiments was probably transported to the Cape Verde Islands during the last ice age when dust fluxes were 15 to 30 times higher than today (Reader et al., 1999) and has been exposed to tropospheric O_3 since then. In the absence of re-activation processes these dust samples would not have been reactive in our laboratory experiments.

From our experiments it is not possible to deduce a definitive uptake coefficient that can be applied to atmospheric chemistry modelling. Our laboratory observations suggest that uptake onto mineral aerosol has a negligible effect on the atmospheric ozone budget because the mineral surface is rapidly passivated. In the real atmosphere, re-activation processes may, however, compete on the same time scale as passivation, which together define the atmospherically relevant uptake coefficient for destruction of O_3 on mineral dust.

Studies in environmental chambers would be most useful to elucidate this problem.

4 Conclusions

The heterogeneous interaction of ozone with authentic Saharan dust surfaces was investigated at room temperature. The steady-state uptake coefficient for uptake of O_3 onto the mineral dust surface was determined to be $\gamma = 7 \times 10^{-6}$ at tropospheric O_3 concentrations. O_3 was destroyed on the (unheated) dust surface and O_2 was produced with a conversion stoichiometry of 1.0. The sample surface could be completely passivated by extended sample exposure to high O_3 concentrations, but sample reactivity could be partially restored overnight.

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